

Article

Thermodynamic Analysis of ORC and Its Application for Waste Heat Recovery

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Abstract: The analysis and optimization of an organic Rankine cycle (ORC) used as a bottoming cycle in the Brayton/ORC and steam Rankine/ORC combined cycle configurations is the main focus of this study. The results show that CO₂ and air are the best working fluids for the topping (Brayton) cycle. Depending on the exhaust temperature of the topping cycle, Iso-butane, R11 and ethanol are the preferred working fluids for the bottoming (ORC) cycle, resulting in the highest efficiency of the combined cycle. Results of the techno-economic study show that combined Brayton/ORC cycle has significantly lower total capital investment and levelized cost of electricity (LCOE) compared to the regenerative Brayton cycle. An analysis of a combined steam Rankine/ORC cycle was performed to determine the increase in power output that would be achieved by adding a bottoming ORC to the utility-scale steam Rankine cycle, and determine the effect of ambient conditions (heat sink temperature) on power increase. For the selected power plant location, the large difference between the winter and summer temperatures has a considerable effect on the ORC power output, which varies by more than 60% from winter to summer.

Keywords: organic Rankine cycle; working fluid properties; thermal efficiency; subcritical ORC; transcritical ORC; combined Brayton ORC cycle; techno-economic analysis

1. Introduction

The increasing global energy demand, energy cost, and sustainability issues bring the need for waste heat recovery and use. According to the U.S. Department of Energy (U.S. DOE), manufacturing industries and power plants produce approximately 60% of the low-temperature waste heat [1]. Releasing the exhaust with temperatures higher than 350 °C directly to the environment represents a large waste of the primary energy. The recovery of exhaust heat and its use through the organic Rankine cycle (ORC) is an efficient and flexible method with simpler structure, higher safety, and lower maintenance requirements compared to the conventional heat recovery methods, such as steam Rankine cycle. Employing the low-grade energy (waste heat) by integrating the ORC into an energy system, such as a power plant, industrial facility, or large diesel engine (or other prime mover) increases the power output and system energy efficiency [2].

An organic working fluid is used in a Clausius–Rankine cycle (ORC), instead of water-steam in a conventional steam Rankine cycle. Due to the low temperature of phase change, organic working fluids represent a good choice for utilization of heat recovered from the low temperature heat sources [3]. In an ORC cycle, the superheated turbine exhaust due to generally lower boiling temperature and evaporation pressure, helps to avoid erosion of the turbine blades caused by the wet steam in a steam Rankine cycle [4]. Performance improvement of a regenerative ORC (ORC with a recuperator) in conjunction with a simple ORC (ORC without a recuperator) is the focus of the recent research work [5].

Due to the remarkable properties of the ORC for waste heat recovery from flue gases, a number of experimental studies were carried out and published in the literature. Zhou et al. [6] used a liquefied

petroleum gas stove as the heat source maintaining the temperature in the range of 90 °C to 220 °C. R123 was chosen as a working fluid and a scroll expander was used to achieve a maximum power output of 0.645 kW and a cycle efficiency of 8.5%. Lemort et al. [7] and Quoilin et al. [8] also used the same working fluid and expander type, reporting the maximum cycle efficiency of 7.4%.

Vatani et al. [9] employed an ORC to recover waste heat from the integrated direct internal reforming-molten carbonate fuel cells (DIR-MCFC) with a pre-reformer. A number of working fluids were used to simulate the cycle at optimum operating conditions resulting in highest thermal efficiency. The results indicate that both the energy and exergy efficiencies were increased by cathode splitting. In addition, a decrease in exergy loss was observed while using cathode splitting for all substances.

Algieri et al. [10] studied the effect of internal heat recovery for sub-, trans- and supercritical ORC with dry working fluids. Mago et al. [11] compared the regenerative ORC based on the combined first and second law of thermodynamics analysis to a simple ORC. The study shows that ORC with dry working fluid not only requires less amount of waste heat to generate specified power output but also lowers irreversibility by increasing cycle efficiency. Acar [12] performed an energy and exergy analysis for the reheat-regenerative Rankine cycle. The results show that, despite the same energy and exergy efficiencies of the closed cycle, exergy analysis yields to a better understanding of the losses in the system. Evaluation of five different ORC was done by Wang et al. [13]. Since a portion of the heat from the turbine exhaust stream is recovered in the recuperator and beneficially used, a regenerative ORC has the lower rate of exergy destruction, compared to the simple cycles.

Hung et al. [14] compared the effect of different types of working fluids on thermal efficiency improvement of the ORCs. The results show that, while the wet and isentropic working fluids do not have a significant effect on thermal efficiency (up to 2% improvements), dry fluids can improve thermal efficiency by more than 9%.

A simple ORC using waste heat sources and different working fluids has been the focus of many papers and studies [15–19]. Saleh et al. [20] compared 31 different working fluids and their effect on the thermal efficiency for an ORC with different work cycle configurations. The effect of different working fluids on thermal efficiency was also studied by Lakew and Bolland [21] for a simple subcritical ORC operating in the 80 °C to 160 °C temperature range.

Numerous criteria are as well as international safety and environmental protocols and agreements are considered during the fluid selection procedure. The ozone depletion potential (ODP), flammability, toxicity and global warming potential (GWP) are the criteria that need to be considered during the working fluid selection process. Papadopoulos et al. [22] used 15 criteria for the fluid selection; with environmental, safety, physical, chemical and economical properties being the five main groups. The best working fluid is selected based on the cycle thermal efficiency. Details are provided in [23].

Since there is no working fluid that satisfies all selection criteria [24], the fluid selection method should balance all the main mentioned criteria. The selection processes is divided into two steps: elimination and ranking [25]. Elimination is used to remove the unsuitable working fluids from the list before the ranking process is applied, having in mind that not all the properties have the same weight of evaluation. Roedder et al. [26] used a combination of the elimination and ranking methods to choose the best working fluid based on the 22 criteria. Iso-butane was identified as the best working fluid for a two-stage ORC.

A combined cycle consists of several thermodynamic cycles, grouped into the topping or high-temperature and the bottoming or low-temperature cycles. Rejected heat from the topping cycle is utilized by the bottoming cycle to produce more power. For a low exhaust temperature of the topping cycle, organic Rankine cycle (ORC) is a suitable choice for the bottoming cycle, which performs better than the steam Rankine cycle [27–29]. The ORC power plants are commercially available on a small scale due to low maximum operating temperature, and are used in renewable energy, geothermal and low-temperature heat recovery applications [27].

Despite the extensive studies on ORC, the combination of a regenerative Brayton cycle as the topping cycle and an ORC as the bottoming cycle, i.e., the combined Brayton/ORC, has not been evaluated to the sufficient level of detail, and warrants more investigation.

This paper is concerned with the exhaust heat recovery from the Brayton and steam Rankine cycles and its use in a simple ORC. The maximum temperature operating range used in this study is between 50 °C and 350 °C, which is well within the ORC operating range. In this temperature range, other cycles such as steam Rankine, Brayton, or Kalina cycles have a very low thermal efficiency. Thus, there is on benefit of using any of these cycles as a bottoming cycle for recovery and utilization of the low-grade waste heat.

The effect of twelve working fluids on cycle performance was studied over the range of cycle operating conditions with the aim to identify the best working fluid for the specified set of operating conditions. The cycle calculations and simulations were performed by employing the Epsilon Professional V11 (EPV-11) power systems modeling software [30]. EPV-11 is professional software used for a detailed design, analysis, and optimization of the power generation systems.

Selection of working fluids resulting in best performance (thermodynamic efficiency or net specific work output) of the ORC for the specified operating conditions (maximum temperature and pressure, heat rejection temperature, and others) is a time-consuming and arduous task, especially when a large number of working fluids is being considered. The commonly used approach involves performing a number of parametric calculations over a range of operating parameters for a number of the candidate working fluids. The results are usually presented in a graphical form, for example: for each of the analyzed working fluids efficiency is plotted as a function of the maximum temperature and pressure. The best working fluid is selected by manually inspecting efficiency diagrams for all analyzed fluids. In addition, since the selection process is manual, there is a certain level of subjectivity and the potential for error involved.

The best (most suitable) working fluid, for use in ORC in waste heat recovery applications, was selected based on the selection procedure developed by the authors and published in the previous studies [31–33]. The working fluid selection procedure allows for a non-subjective and exact determination of the best working fluid for the selected cycle operating conditions, as well as construction of performance maps which provide visual and easy-to-interpret information on the cycle thermal performance and the best working fluids. This selection procedure was applied to determine the best working fluids for the combined regenerative Brayton/ORC and steam Rankine/ORC applications.

A techno-economic analysis of the ORC and combined Brayton/ORC cycles was performed to determine the total capital investment and levelized cost of electricity (LCOE), and allow economic comparison of the investigated cycles.

2. Thermodynamic Modeling and Working Fluid Properties

The operating principle of the ORC and steam Rankine cycles are the same: compression of the liquid, phase change (evaporation) in the evaporator, expansion in the turbine (expander), and phase change (condensation) in the condenser [34]. The main components involved in a simple ORC (feed pump, evaporator, turbine, and condenser) are presented in Figure 1. The working fluid is delivered to the evaporator by the feed pump where it is evaporated at approximately constant pressure using the externally supplied heat. In some ORC designs, a superheater is used to superheat the working fluid [4]. The saturated or superheated working fluid is expanded in the turbine (expander), which is driving an electric generator. The low-pressure, low-temperature working fluid leaving the turbine is condensed in the condenser. The pressure of the working fluid leaving the condenser as a saturated (or slightly subcooled liquid) is increased by the feed pump, completing the power cycle.

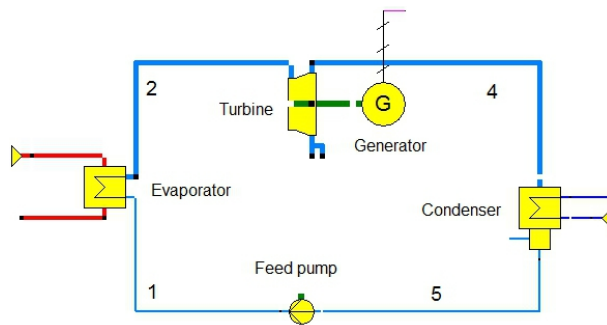


Figure 1. Schematic of a simple ORC.

The temperature-specific entropy (T-s) diagrams of simple subcritical and transcritical ORCs are presented in Figure 2. There is no phase change in the supercritical cycle where the working fluid remains as a homogeneous supercritical fluid throughout the entire power cycle.

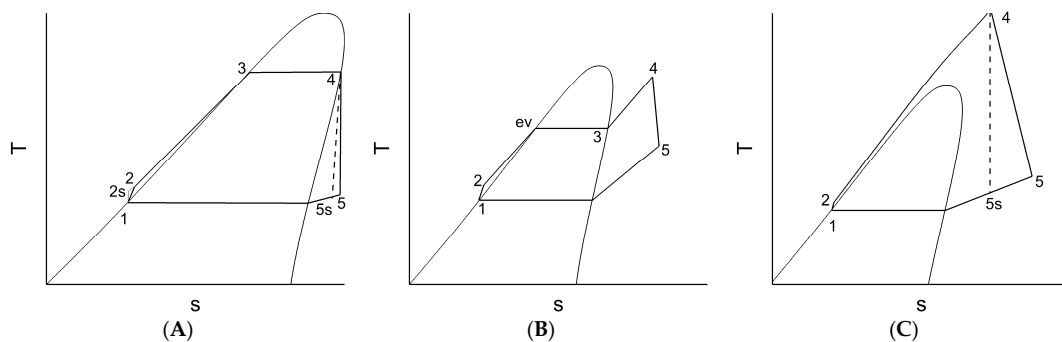


Figure 2. T-s diagram for a simple ORC: (A) subcritical; (B) subcritical with superheat; and (C) transcritical.

The main components of a regenerative Brayton/simple ORC are shown in Figure 3.

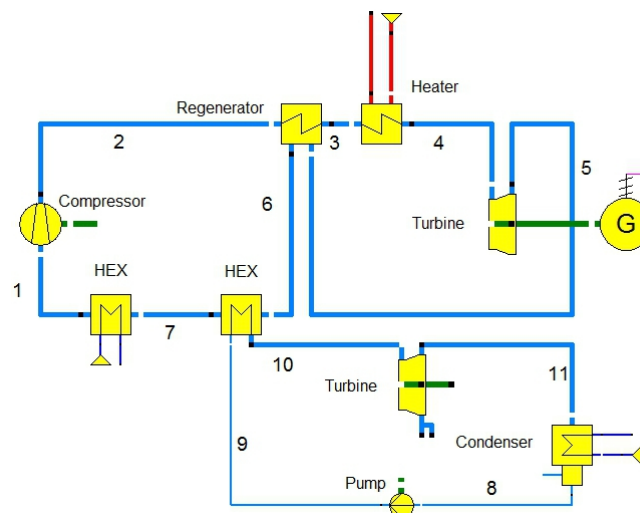


Figure 3. Schematic representation of a combined regenerative Brayton/ORC cycle.

In a combined power cycle, two or more thermodynamic cycles are combined to achieve higher efficiency and power output. Based on the operating temperature range, the cycles are divided into the topping and bottoming cycles. The Brayton cycle was selected as a topping cycle because the

high turbine inlet temperature (TIT) is needed to achieve high thermal efficiency [34]. The exhaust temperature of a simple Brayton cycle (above 400 °C) is higher than the maximum allowed ORC operating temperature; thus, a regenerative Brayton cycle, having lower exhaust temperature, was used as a topping cycle in a combined Brayton/ORC cycle in this study.

2.1. Thermodynamic and Environmental Properties of the Working Fluids

Selection of the working fluid for the ORC has an important role on the cycle performance. Twelve working fluids were analyzed in this study. Based on previous studies, the working fluids selected for the analysis have the potential to give a good ORC performance [31–33]. Based on the slope of the saturated vapor curve in the T-s diagram (Figure 4), working fluids are divided into three main groups: dry, wet, and isentropic. The positive, negative, and infinite slope refers to the dry, wet, and isentropic fluids, respectively. In an ORC, the slope of the saturated vapor curve is one of the most important thermophysical properties of the working fluid, having a significant impact on thermal efficiency and equipment arrangement [14]. The wet working fluid has to be superheated before its expansion in the turbine to maintain the maximum allowed wetness at the turbine outlet and avoid erosion damage to the turbine blading [35]. Previous studies on the isentropic fluids [35] have shown that there is not a strong relationship between the cycle efficiency and turbine inlet temperature (TIT).

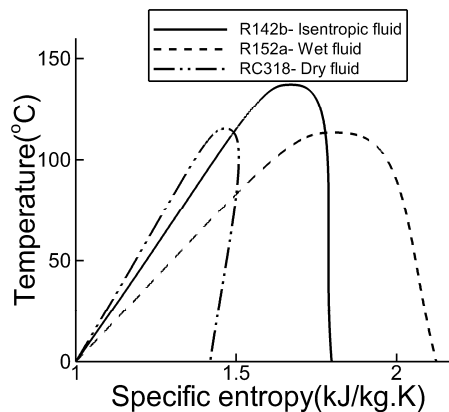


Figure 4. Wet, dry and isentropic fluids.

For dry fluids, the highest cycle efficiency is achieved by maintaining the saturated steam conditions at the turbine inlet [11,36,37]. Superheating the dry fluid will increase the turbine exit temperature and condenser loading without having a significant impact on the turbine power output.

During the plant design, the environmental and safety characteristics of working fluids should also be considered because they play a significant role on the plant operators' health and the environment. Some of the environmental and safety data for the selected working fluids are shown in Table 1. P_{cr} and T_{cr} are the critical pressure and temperature of the working fluids.

The properties of working fluids considered in this study are the global warming potential (GWP), ozone depletion potential (ODP), toxicity, flammability, and corrosiveness. The GWP of a working fluid is a measure of its effect on Global Warming. Carbon dioxide (CO_2) has been assigned a GWP of 1. Thus, a fluid with GWP of 2 has the effect on global warming two times stronger compared to the CO_2 . Working fluids which have higher ODP than zero cannot be considered for power generation due to restrictions on their use imposed by the Montreal protocols [38]. The properties in Table 1 were obtained from the GESTIS database [39]. As can be seen in Table 1, ammonia is not a good choice of the working fluid for power generation due to its toxicity, flammability, and corrosiveness.

Selection of the working fluid for a regenerative Brayton cycle used as a topping cycle in a combined Brayton/ORC cycle has a significant effect on performance. Nine working fluids were evaluated in this study to determine the best working fluid for the topping cycle. Table 2 shows the

properties of the working fluids used in this study. Based on previous studies, these working fluids have the potential for good performance in a regenerative Brayton cycle [32].

Table 1. Physical, safety and environmental data of working fluids for ORC.

	Fluid	Physical Data				Environmental and Safety Data				
		Molar Mass (kg/kmol)	T_{cr} (°C)	P_{cr} (MPa)	Type	GWP	ODP	Toxicity	Flamm-Ability	Corrosi-Venous
1	Butane	58.122	151.9	3.79	Dry	3	0	NO	YES	NO
2	Iso-butane	58.122	134.6	3.62	Dry	3	0	NO	YES	NO
3	Ammonia	17.03	132.2	11.33	Wet	0	0	YES	NO	YES
4	R11	137.37	197.9	4.40	Isentropic	4000	1	NO	NO	NO
5	R141b	116.95	204.3	4.21	Isentropic	600	0.11	YES	NO	NO
6	R152a	66.051	113.2	4.51	Wet	140	0	NO	YES	NO
7	R142b	100.5	137.1	4.05	Isentropic	1800	0.065	YES	YES	NO
8	R134a	102.03	101.0	4.05	Wet	1300	0	NO	NO	NO
9	Ethanol	46.068	240.7	6.14	Wet	n.a.	n.a.	NO	YES	NO
10	R113	187.38	214.0	3.39	Dry	6130	1	NO	NO	NO
11	Iso-pentane	72.149	187.2	3.37	Dry	5	0	YES	YES	NO
12	R114	170.92	145.6	3.25	Dry	10.04	1	NO	NO	NO

n.a., non-available.

Table 2. Physical data of the working fluids for a topping regenerative Brayton cycle.

	Fluid	Molar Mass (kg/kmol)	T_{cr} (°C)	P_{cr} (MPa)
1	Air	28.965	−140.62	3.78
2	CO ₂	44.01	30.978	7.37
3	N ₂	28.013	−146.96	3.39
4	He	4.0026	−267.95	0.22
5	O ₂	31.999	−118.57	5.04
6	Methane	16.043	−82.586	4.59
7	Ne	20.179	−228.66	2.67
8	Ar	39.948	−122.46	4.86
9	Kr	83.798	−63.67	5.52

2.2. Calculation of Thermal Efficiency

The analysis of the cycle performance was performed by neglecting the friction and heat losses in the pipes and heat exchangers, and assuming adiabatic turbomachinery (turbine and feed pump). An ORC is a considerably simpler and smaller power cycle compared to the Steam Rankine cycle with significantly smaller heat exchangers and considerably simpler connecting piping.

In addition, the molar mass of most organic fluids and their density are higher compared to steam, resulting in comparatively smaller volumetric flows and, thus smaller equipment. Thus, friction in the pipes and heat exchangers, and the resulting pressure drop, does not have a significant effect on cycle performance and can be neglected.

Different working fluids have different densities, which results in a difference in equipment size (for example CO₂ vs. He). To include the difference in equipment size in the analysis, thermodynamic evaluation was supplemented by the techno-economic analysis to compare the capital investment costs, and the levelized cost of electricity (LCOE).

Regarding the heat losses, turbomachinery is typically assumed to be adiabatic since any heat exchange with the surroundings is several orders of magnitude smaller compared to the energy flux through the turbomachine. The heat exchangers and connecting piping in the ORC are relatively small and, thus can be well insulated, minimizing heat losses.

2.2.1. Thermal Efficiency of a Simple ORC

Based on the previous studies performed by the authors [31,32], thermal efficiency of a subcritical ORC without a superheat can be calculated as:

$$\eta_{th} = \eta_t(c_1 \times FOM + c_2) \quad (1)$$

$$C_1 = 1.207T_{EC}^2 - 3.973T_{EC} + 2.831 \quad (2)$$

$$C_2 = -1.862T_{EC}^2 + 5.824T_{EC} - 4.009 \quad (3)$$

where η_t and FOM are turbine isentropic efficiency and figure of merit, respectively. FOM is expressed by:

$$FOM = Ja^{0.1} \left(\frac{1}{T_{EC}} \right)^{0.8} \quad (4)$$

$$Ja = \frac{\bar{C}_{P,13}(T_4 - T_1)}{h_{fg}} \quad (5)$$

$$T_{EC} = \frac{\text{Evaporation temperature}}{\text{Condensation temperature}} = \frac{T_4}{T_1} \quad (6)$$

where $\bar{C}_{P,13}$ represents the average specific heat capacity calculated from the State Point (SP) 1 to SP 3, T_1 is the temperature at the feed pump inlet, T_4 is the maximum temperature (turbine inlet temperature, TIT), and h_{fg} is the latent heat (enthalpy) of evaporation (vaporization). The quantity Ja is the Jacob number defined as the ratio of the sensible and latent heats.

As can be seen in Equation (1), there is a linear relationship between FOM and η_{th} . According to Equations (1) and (4), η_{th} decreases as the Jacob number increases. Details are provided in [31,32]. Based on the results, the following expression for the specific heat input for a subcritical ORC without a superheat was developed:

$$\frac{\dot{q}_{in}}{\dot{m}} = h_{fg}(Ja + 1) \quad (7)$$

where \dot{m} is mass flow rate of the power cycle.

Compared to a subcritical cycle without a superheat, thermal efficiency of a superheated subcritical cycle is affected by an additional variable; the superheat temperature. The following expression for thermal efficiency of a superheated ORC was proposed by the authors [31,32]

$$\eta_{th} = \eta_t(c_1 Ja_t + c_2) \quad (8)$$

$$Ja_t = (Ja + k \times Ja_s)^{1.45} \quad (9)$$

$$c_1 = \frac{(c_{11} \times \frac{T_4}{T_1} + c_{12} + \left(\frac{T_{ev}}{T_1}\right)^{11})}{82.875 \left(\frac{T_4}{T_{ev}}\right)^{1.46T_{ev}-41.9199}}, \quad c_2 = \frac{(c_{21} \times \frac{T_4}{T_1} + c_{22} + \left(\frac{T_{ev}}{T_1}\right)^{0.1})}{82.875 \left(\frac{T_4}{T_{ev}}\right)^{-0.44}} \quad (10)$$

$$c_{11} = -0.5195T_1 + 121.44, \quad c_{12} = 0.5953T_1 - 146.88 \quad (11)$$

$$c_{21} = -0.5157T_1 + 225.92, \quad c_{22} = 0.5179T_1 - 243.95 \quad (12)$$

where $k = 1$ for the wet and isentropic fluids, while for the dry fluids $k = 1.5$ [31]. Ja is the Jacob number and Ja_s is the superheat Jacob number.

$$Ja = \frac{\bar{C}_{P,1ev}(T_{ev} - T_1)}{h_{fg}}, \quad Ja_s = \frac{\bar{C}_{P,34}(T_4 - T_{ev})}{h_{fg}} \quad (13)$$

The results show that thermal efficiency decreases as the Jacob number Ja and superheat Jacob number Ja_s increase. Based on the results, the following expression for the specific heat input for a subcritical ORC with a superheat was developed:

$$\frac{\dot{q}_{in}}{\dot{m}} = h_{fg}(Ja + Ja_s + 1) \quad (14)$$

For the supercritical ORC shown in Figure 2C, a similar procedure was used to determine expression for thermal efficiency:

$$\eta_{th} = \eta_t(c_1 T_{md} + c_2) \quad (15)$$

$$T_{md} = \ln(T_{EC}) - 0.8 \times k(T_r - 1) \quad (16)$$

$$c_1 = 5.421T_r^3 - 18.332T_r^2 + 20.901T_r - 7.483 \quad (17)$$

$$c_2 = 3.272T_r^3 - 11.065T_r^2 + 12.454T_r - 4.63 \quad (18)$$

$$T_r = \frac{T_4}{T_{cr}} \quad (19)$$

where T_{cr} and T_{md} are the critical and modified temperatures of the working fluid, respectively. The constant k has the same value as for a subcritical ORC with the superheat. For a transcritical ORC, as shown by Equation (15), at the critical point of the analyzed working fluids, thermal efficiency is a linear function of the dimensionless temperature T_r .

Based on the results, the following expression for the specific heat input for a transcritical ORC with the superheat was developed:

$$\frac{\dot{q}_{in}}{\dot{m}} = c_{p14}(T_4 - T_1) \quad (20)$$

Finally, the net work output of all types of a simple ORC can be calculated as:

$$\dot{W}_{net} = \eta_{th}\dot{q}_{in} \quad (21)$$

2.2.2. Thermal Efficiency of a Combined Regenerative Brayton/ORC

Thermal efficiency of a combined cycle may be calculated as:

$$\eta_{combined} = \frac{\dot{W}_{net, Brayton} + \dot{W}_{net, ORC}}{\dot{q}_{in, Brayton}} = \eta_{th, Brayton} + A \quad (22)$$

Equation (22) provides insight into why combined cycles are more efficient compared to the simple cycles: efficiency of the combined cycle is a sum of the Brayton (topping) cycle efficiency and a positive quantity A . As will be shown later, the value of quantity A depends on selection of the working fluid for the bottoming (ORC) cycle.

Based on the developed correlations and previous results [31,32], twelve working fluids listed in Table 1 have been selected for this study. The use of these working fluids in a simple ORC has a potential to increase thermal efficiency and net power output compared to the other working fluids.

3. Power Block Cost Estimation

The capital cost of a power block consists of the purchased cost of equipment, the labor and materials needed for the installation, such as the piping, the foundations and structural supports, the electrical equipment, the instrumentation and controls, and the indirect expenses. The indirect expenses cover the transportation costs for shipping equipment to the plant site, and salaries for the project personnel.

Table 3 shows components of the total capital investment cost considered in this study. More details can be found in [40].

The bare module cost, C_{BM} , is the sum of direct and indirect costs for each unit as described in Turton et al. [41], and can be calculated by Equation (23).

$$C_{BM} = C_P^0 F_{BM} \quad (23)$$

C_p^0 is purchase cost of equipment in base conditions. Base condition represents the case where the equipment is made of the most common material, usually carbon steel operating at ambient pressure. F_{BM} is the bare module factor.

The data for the purchase cost of the equipment described in Turton et al. [41] were obtained based on the average CEPCI (Chemical Engineering Plant Cost Index) value of 397. The updated value of CEPCI of 556.8 for the year of 2015 was utilized for the present economic estimate.

The purchased equipment cost for base conditions, C_p^0 may be determined by employing Equation (24).

$$\log_{10} C_p^0 = K_1 + K_2 \times \log_{10} AA + K_3 (\log_{10} AA)^2 \quad (24)$$

where AA is the size parameter for the equipment, and K_1 , K_2 , and K_3 are constants given in Table 4.

Table 3. Components of the total capital investment.

Components of Total Capital Investment		Formula
C_{TCI}	Total capital investment	$C_{TCI} = C_{TDC} + C_{land} + C_{royal} + C_{startup}$
$C_{startup}$	Cost of plant startup	$C_{startup} = 0.1 \times C_{TDC}$
C_{royal}	Cost of royalties	0
C_{land}	Cost of land	$C_{land} = 45 \times 10^4 \times (P/100MWNET)^{0.7}$
C_{TDC}	Total depreciable capital	$C_{TDC} = 1.18 \times C_{DPI}$
C_{DPI}	Total direct permanent investment	$C_{DPI} = 1.1 \times C_{TBM}$
C_{TBM}	Total bare module cost	$C_{TBM} = \sum C_{BM} + C_{spare} + C_{wf}$
C_{wf}	working fluid	C_{wf}
C_{SPARE}	Cost for spares	$2.1 C_{BM}^{pump}$

Table 4. Coefficients used to calculate the price of different components in a power block.

Equipment	K_1	K_2	K_3	C_1	C_2	C_3	B_1	B_2	F_M	F_{BM}	AA
ORC turbine	2.2476	1.4965	−0.1618	**	**	**	**	**	**	6.1	kW
ORC pump	3.3892	0.0536	0.1538	−0.393	0.3957	−0.0022	1.89	1.35	1.5	**	kW
ORC HEX	4.3247	−0.0303	0.1634	0.0388	−0.1127	0.0818	1.63	1.66	1	**	Area (m ²)
Motor pump	2.4604	1.4191	−0.1798	**	**	**	**	**	**	1.5	kW
ORC ACC HEX	4.0336	0.2341	0.0497	0.0388	−0.1127	0.0818	0.96	1.21	1	**	Area (m ²)
ORC ACC fan	3.1761	−0.1373	0.3414	**	**	**	**	**	2.5	5	Q(m ³ /s)
motors fans	2.4604	1.4191	−0.1798	**	**	**	**	**	**	1.5	kW
Brayton HEX	0.9420	0.8778	0	**	**	**	**	**	**	**	UA (W/K)
Brayton turbine	3.5195	0.5886	0	**	**	**	**	**	**	**	kW
regenerator	0.716	0.8933	0	**	**	**	**	**	**	**	UA (W/K)
Brayton cooler	1.4843	0.8919	0	**	**	**	**	**	**	**	UA (W/K)
compressor	3.1093	0.9142	0	**	**	**	**	**	**	**	kW
Generator	**	**	**	**	**	**	**	**	**	1.5	kW
Working fluid	**	**	**	**	**	**	**	**	**	1.25	**

Note: **, Value is not needed.

For the Brayton cycle analyzed in this paper, the primary heat exchanger is assumed to be a printed-circuit heat exchanger (PCHE). The high-pressure gas on the cold side and high-viscosity fluid on the hot side are considered for the PCHE. To represent the power density of different working fluids, the compressor data were modified by the density ratio ρ_{air}/ρ_{fluid} . The A-frame, finned-tube air coolers were considered for all cooling processes.

The purchased equipment cost of the electrical generator, $C_{P,gen}^0$ is calculated according to Equation (25) as presented in Ref. [42]

$$C_{P,gen}^0 = 690(\dot{W}_{gen})^{0.95} \quad (25)$$

The bare module factor, F_{BM} was calculated from:

$$F_{BM} = B_1 + B_2 \times F_M \times F_P \quad (26)$$

$$\log_{10} F_P = C_1 + C_2 \times \log_{10} P + C_3 (\log_{10} P)^2 \quad (27)$$

where B_1 and B_2 are constants given in Table 4; F_M is equipment material factor listed in Table 4; and F_P is the operating pressure factor. The relative pressure having unit of bar gauge (1 bar = 0.0 barg) is used in Equation (27), where pressure factors are always greater than unity. The constants C_1 , C_2 and C_3 are given in Table 4. Since the ORC is running at temperatures lower than 350 °C, material changes were not considered for the components operating at different temperatures. The Brayton cycle operating temperature range is between 300 °C and 1000 °C, thus materials such as carbon steel, stainless steel, nickel alloys 625, 718, etc. need to be used for different operating temperatures. The material selection method for the expanders and heat exchanges is discussed in [43]. Tables 5–7 show F_{BM} value for components of the Brayton cycle operating at different maximum temperatures and pressures.

Table 5. Material selection for the primary heat exchanger and compressor in a Brayton cycle.

T_{max} (°C) <	$P_{max} < 10$ MPa		$P_{max} < 20$ MPa		$P_{max} < 30$ MPa	
	Material	F_{BM}	Material	F_{BM}	Material	F_{BM}
500	Carbon steel	1	Carbon steel	1	Carbon steel	1
650	Stainless steel (347)	2.5	Stainless steel (347)	2.5	Stainless steel (347)	2.5
700	Stainless steel (347)	2.5	Stainless steel (347)	2.5	Nickel alloy(625)	3
750	Stainless steel (347)	2.5	Nickel alloy (625)	3	Nickel alloy (625)	3
900	Nickel alloy (625)	3	Nickel alloy (625)	3	Nickel alloy (625)	3

Table 6. Material selection for the turbine in a Brayton cycle.

T_{max} (°C) <	$P_{max} < 10$ MPa		$P_{max} < 20$ MPa		$P_{max} < 30$ MPa	
	Material	F_{BM}	Material	F_{BM}	Material	F_{BM}
500	Stainless steel (347)	2.5	Stainless steel (347)	2.5	Stainless steel (347)	2.5
650	Stainless steel (347)	2.5	Nickel alloy (625)	3	Nickel alloy (625)	3
900	Nickel alloy (625)	3	Nickel alloy (625)	3	Nickel alloy (625)	3

Table 7. Material selection for the air-cooled cooler in a Brayton cycle.

T_{max} (°C) <	$P_{max} < 10$ MPa		$P_{max} < 20$ MPa		$P_{max} < 30$ MPa	
	Material	F_{BM}	Material	F_{BM}	Material	F_{BM}
500	Carbon steel	1	Carbon steel	1	Carbon steel	1
650	Carbon steel	1	Stainless steel (347)	2.5	Stainless steel (347)	2.5
900	Stainless steel (347)	2.5	Stainless steel (347)	2.5	Stainless steel (347)	2.5

The pumps are inexpensive but require maintenance to prevent leaks, therefore it is often recommended to provide funds for spares, C_{spare} , for the pumps [40].

The cost of land, C_{land} , is related to size of power block [44] and is assumed to be 2.47 \$/m² in southern California while the cost of royalties, C_{royal} , is neglected in the present work.

The cost of the working fluid, C_{wif} should be considered as the capital cost for an ORC. The amount of the working fluid needed may be expressed as the volume of liquid required to fill the whole ORC process [45]. Toffolo et al. [46], showed that about 370 kg of Iso-butene are needed for each kg/s of the working fluid for an ORC. More details can be found in [46]. For the Brayton cycle, the cost of the working fluid does not play a major role on the cost of the power block. Table 8 shows the price of working fluids for ORC and Brayton cycles.

The total operation and maintenance cost, C_{OM} , is the sum of the direct manufacturing cost, C_{DMC} , and fixed costs, C_{Fix} .

$$C_{OM} = C_{DMC} + C_{Fix} \quad (28)$$

$$C_{DMC} = C_{Main} + C_{UT} \quad (29)$$

The sum of the maintenance cost and utilities cost, which includes wages and benefits, salaries and benefits, materials and services, and manufacturing overhead is called the direct manufacturing cost.

As defined in Ref. [40], maintenance cost C_{Main} can be calculated as:

$$C_{Main} = 0.0805C_{TCI} \quad (30)$$

Utilities cost is related to the dry cooling tower [44] and it is calculated as:

$$C_{UT} = 2.1795 \times (\dot{W}_{net}(MW))^{0.7} \quad (31)$$

Fixed cost includes cost of property taxes and liability insurance is equal to:

$$C_{Fix} = 0.02C_{TDC} \quad (32)$$

Annual operation hours and electricity generation are:

$$OH_{Annual} = CF \times 24 \times 365 \quad (33)$$

$$E_{net} = \dot{W}_{net} \times OH_{Annual} \quad (34)$$

where CF is the capacity factor of the power block and it is assumed to be 0.8. The Levelized Cost of Electricity (LCOE) of the project is calculated according to Equation (35) as described in [44]:

$$LCOE = \frac{C_{TCI} + \sum_{n=1}^N \frac{C_{OM,n}}{(1+d_{nominal})^n}}{\sum_{n=1}^N \frac{E_{net,n}}{(1+d_{real})^n}} \quad (35)$$

$$d_{nominal} = \left(\left(1 + \frac{d_{real}}{100} \right) \times \left(1 + \frac{r}{100} \right) - 1 \right) \times 100 \quad (36)$$

where d is the discount rate and r is the inflation rate. The real discount and interest rates were assumed to be 0.055 and 0.025, respectively. N is economical lifetime of plant set to be 20 years, while n is the year of operation.

Table 8. Price of different working fluids.

Fluid	Price (\$/kg)
Air	0
Butane	1.195
CO ₂	0.1
Ethanol	0.53
Helium	42.553
Iso-butane	0.86
R11	3.60
R141b	1.75

4. Results and Discussion

As explained earlier, the analysis of cycle performance was performed by neglecting the friction and heat losses in the pipes and heat exchangers, and assuming adiabatic turbomachinery (turbine and feed pump).

4.1. Effect of Working Fluid Properties on Thermal Efficiency and Specific Net Work Output

Correlations for thermal efficiency developed by the authors [31,32] were used to investigate the effects of the working fluid properties on performance of a simple ORC. Equations (1), (5) and (8) show that, in a subcritical region, thermal efficiency is a function of the specific heat capacity and the latent heat of evaporation.

It can be shown that the first derivative of Equations (1) and (8) with respect to C_p in the subcritical region is negative (Equation (37)), meaning that at constant maximum and minimum temperatures, working fluids with higher specific heat capacity give lower thermal efficiency.

$$\frac{\partial \eta_{th}}{\partial C_p} < 0 \quad (37)$$

However, the first derivative of Equations (1) and (8) with respect to h_{fg} in the subcritical region is positive (Equation (38)), meaning that at constant maximum and minimum temperatures, working fluids with higher latent heat of evaporation give higher thermal efficiency.

$$\frac{\partial \eta_{th}}{\partial h_{fg}} > 0 \quad (38)$$

Since the first derivatives of expression for \dot{W}_{net} (Equation (21)) with respect to specific heat capacity C_p and latent heat of evaporation h_{fg} in the subcritical region are positive, Equation (39), working fluids with higher C_p or h_{fg} produce higher net power output.

$$\frac{\partial \dot{W}_{net}}{\partial C_p} > 0, \frac{\partial \dot{W}_{net}}{\partial h_{fg}} > 0 \quad (39)$$

The effect of critical temperature on thermal efficiency (Equations (1) and (8)) and net power output (Equation (21)) for $T_{min} = 2^\circ\text{C}$ and $T_{max} = 100^\circ\text{C}$ is presented in Figure 5. As the results show, both η_{th} and \dot{W}_{net} increase as the latent heat of evaporation is increased. An increase in the specific heat, C_p , results in a higher net power output and lower thermal efficiency.

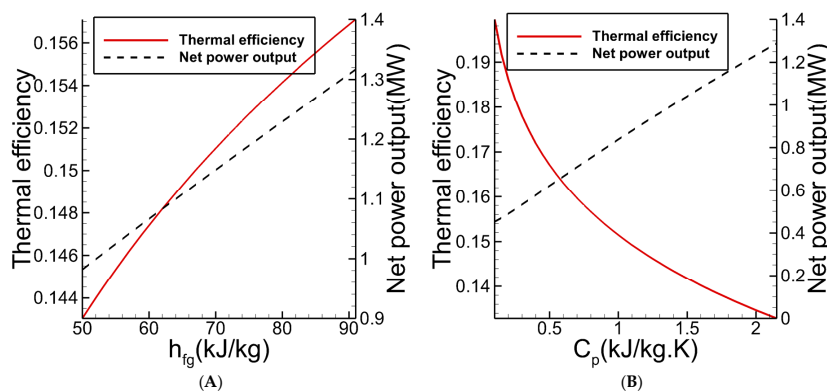


Figure 5. Effect of latent heat of evaporation and specific heat capacity on thermal efficiency and net power output of a simple ORC in the subcritical region: (A) h_{fg} ; and (B) C_p .

Depending on the application of a simple subcritical ORC, there is an optimum specific heat capacity representing a tradeoff between thermal efficiency and net power output. The optimal value of C_p may be determined by developing a relationship between the LCOE and C_p and finding its minimum.

Equation (15) shows that in the supercritical region, thermal efficiency is affected by the critical temperature T_{cr} . It can be shown that the first derivative of Equation (15) in the supercritical region is

positive (Equation (40)), meaning that at constant maximum and minimum temperatures, working fluids with higher critical temperature give higher thermal efficiency.

$$\frac{\partial \eta_{th}}{\partial T_{cr}} > 0 \quad (40)$$

Since the first derivatives of the expression for the net power output (Equation (21)) with respect to the specific heat C_p and critical temperature T_{cr} (expressed in dimensionless form as T_r) are positive, Equation (41), working fluids with higher C_p or T_{cr} produce higher net power output.

$$\frac{\partial \dot{W}_{net}}{\partial C_p} > 0, \frac{\partial \dot{W}_{net}}{\partial T_{cr}} > 0 \quad (41)$$

In addition, the first derivative of Equations (8), (15) and (21) with respect to k in the superheated subcritical and supercritical region is negative (Equation (42)), meaning that, at constant maximum and minimum temperatures, wet and isentropic working fluids give higher thermal efficiency and net power output, compared to the dry fluids.

$$\frac{\partial \eta_{th}}{\partial k} < 0, \frac{\partial \dot{W}_{net}}{\partial k} < 0 \quad (42)$$

The effect of critical temperature on thermal efficiency (Equation (15)) and net power output (Equation (21)) for $T_{min} = 2^\circ\text{C}$ and $T_{max} = 200^\circ\text{C}$ is presented in Figure 6. As the results show, both η_{th} and \dot{W}_{net} increase as critical temperature is increased.

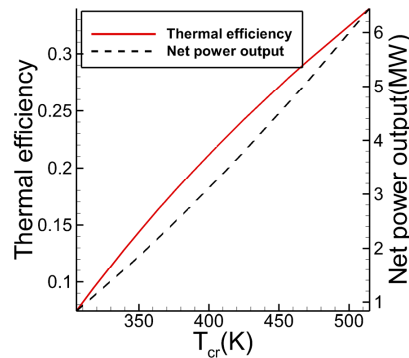


Figure 6. Effect of critical temperature on thermal efficiency and net power output of a simple ORC in the supercritical region.

4.2. The Effect of Operating Conditions on Performance of a Combined Brayton/ORC Cycle

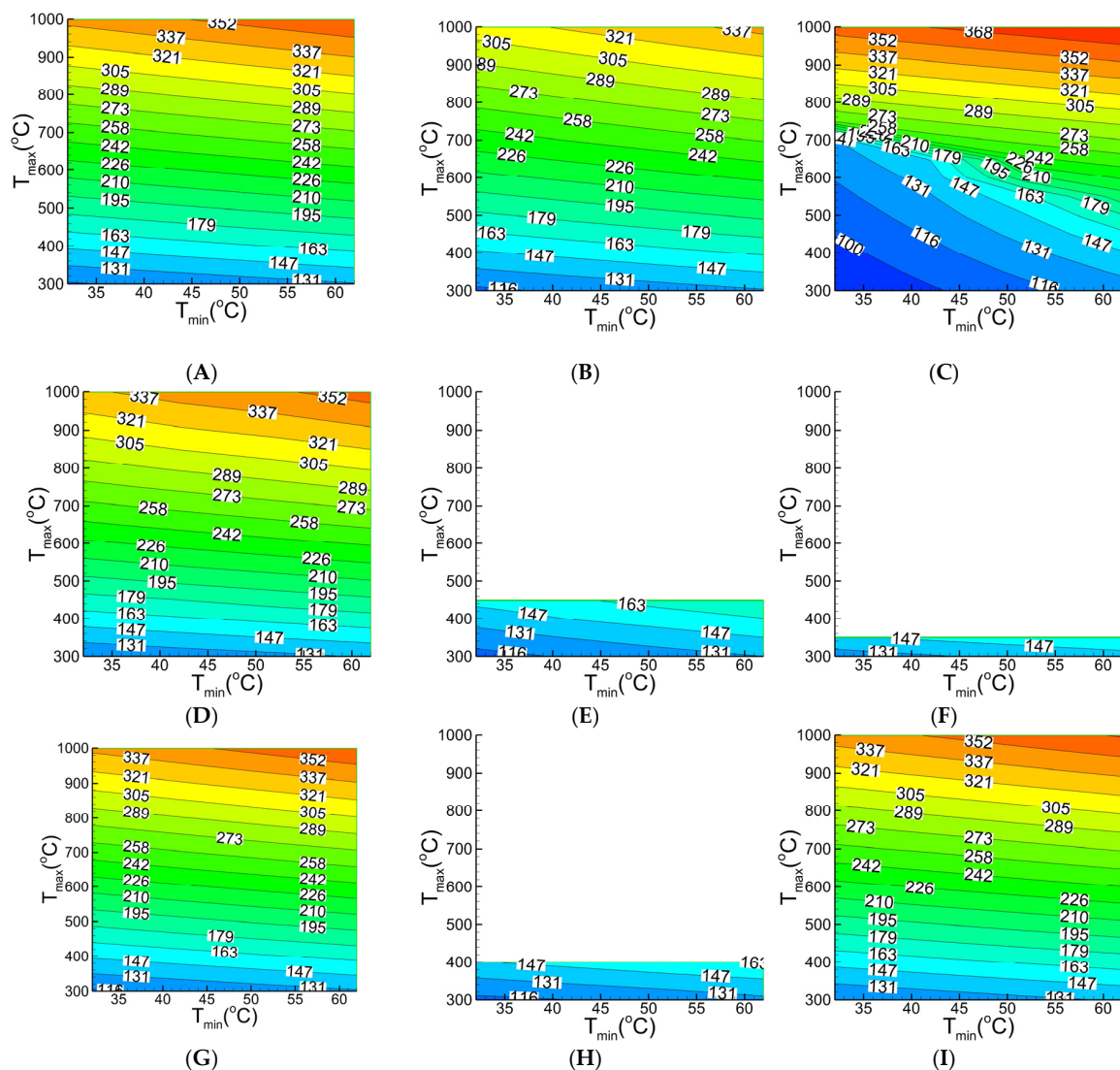
Thermal efficiency of a combined regenerative Brayton/ORC cycle, shown in Figure 3, was determined over a range of operating conditions for twelve working fluids listed in Table 1 for the bottoming (ORC) cycle, and nine working fluid listed in Table 2 for the topping regenerative Brayton cycle. The cycle parameters used in the calculations are summarized in Table 9.

The temperature difference between the topping cycle turbine inlet temperature (TC-TIT) and the heat source temperature of 10°C was assumed in the calculations. In addition, the optimal pressure ratio of the topping cycle was determined, as described in [47]. At the optimal pressure ratio, the cycle network output reaches its maximum value. Since the flow rate of the working fluid in the bottoming cycle is dependent on the mass flow rate of the working fluid in the topping cycle, a constant gross power output of 100 MW was assumed for the topping cycle.

The topping (regenerative Brayton) cycle exhaust (heat rejection) temperature (T_6) for nine working fluids is presented in Figure 7 over the range of operating conditions.

Table 9. Cycle parameters for a combined regenerative Brayton/ORC cycle.

Parameter	Value	Reference
Brayton cycle turbine isentropic efficiency	0.90	[34]
ORC turbine isentropic efficiency	0.87	[34]
Compressor and pump isentropic efficiency	0.80	[34]
P_2 (MPa)	5–30	Assumed
T_1 (°C), T_8 (°C)	32–62	Assumed
T_3 (°C)	300–1000	Assumed
Effectiveness	0.85	[34]
Upper temperature difference for HEX (°C)	10	Assumed
P_{10} (MPa), $T_{10} > T_{cr}$	P_{cr}	Assumed
P_{10} (MPa), $T_{10} < T_{cr}$	P_{sat}	Assumed

**Figure 7.** Topping cycle exhaust temperature for nine working fluids: (A) Air; (B) Ar; (C) CO₂; (D) He; (E) Kr; (F) Methane; (G) N₂; (H) Ne; and (I) O₂.

As the results show, depending on the operating conditions, the topping cycle using CO₂ as a working fluid has the highest and lowest cycle exhaust temperature, followed by air and O₂. For example, for a TIT of 1000 °C, CO₂ produces the cycle exhaust temperature around 350 °C. For the range of analyzed operating conditions, the exhaust temperature of the regenerative CO₂ Brayton

cycle is between 100 °C and 350 °C, which is within the ORC operating range. Thus, the ORC can be selected as the bottoming cycle in the combined regenerative Brayton/ORC cycle configuration.

Figure 8 shows the effect of exhaust temperature of the topping cycle (TC-ET) on the A value given in Equation (22), where quantity A represents improvement in thermal efficiency of the combined cycle with respect to the topping cycle. Five working fluids having the highest A value (efficiency improvement with respect to the topping cycle) are shown in Figure 8. As can be seen in Figure 8, for the values of topping cycle exhaust temperature lower than 227 °C, Iso-butane performs better than other working fluids. R11 is the preferred working fluid for TC-ET in the 227 °C and 327 °C range. For TC-ET higher than 327 °C, ethanol gives the highest A value (highest efficiency improvement).

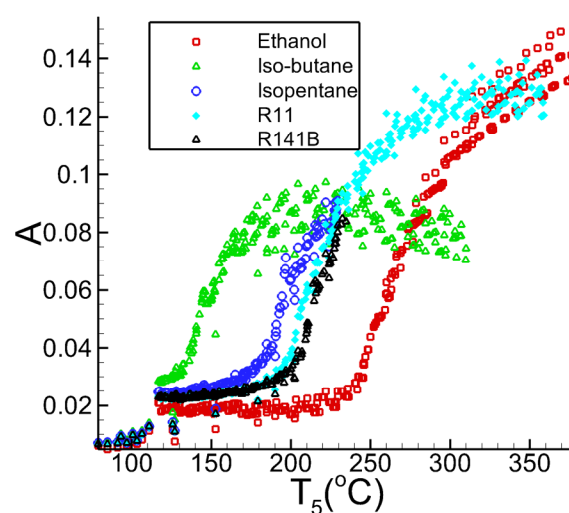


Figure 8. Effect of the topping cycle exhaust temperature on thermal efficiency improvement of a combined regenerative Brayton/ORC cycle relative to the topping regenerative Brayton cycle.

One of the main objectives of this study is selection of the preferred (most suitable, best) working fluid(s) for the given cycle operating conditions. A performance map of thermal efficiency for the combined regenerative Brayton/ORC cycle was developed to enable selection of the best working fluids for the topping and bottoming cycles, Figure 9.

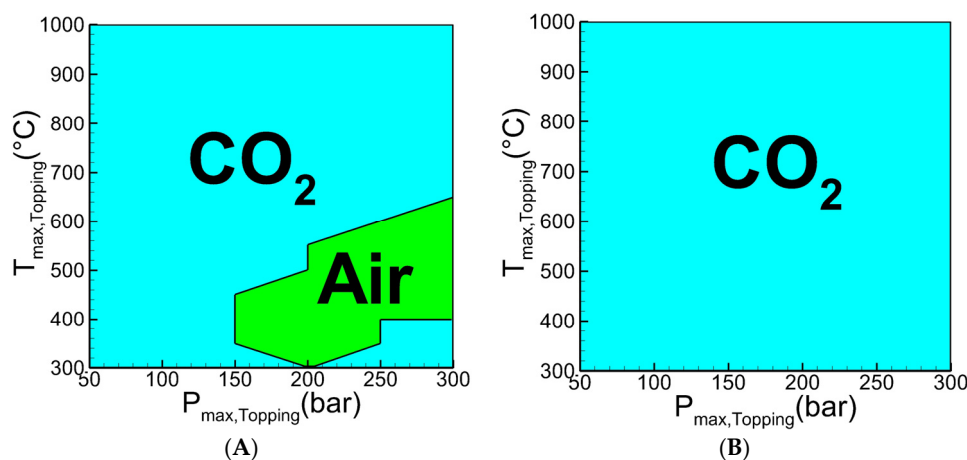


Figure 9. Cont.

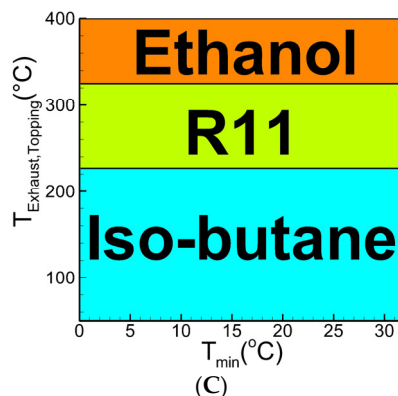


Figure 9. Performance map of thermal efficiency for a combined regenerative Brayton/ORC cycle: (A) topping cycle for $T_{min} < 42$ °C; (B) topping cycle for $T_{min} > 42$ °C; and (C) bottoming cycle.

Performance maps for the topping cycle are presented in Figure 9A,B. As shown in Figure 9A, for the minimum temperature of the combined regenerative Brayton/ORC cycle lower than 42 °C, depending on the maximum temperature and pressure, CO₂ or air are the preferred working fluids. As shown in Figure 9B, for the minimum temperature higher than 42 °C, CO₂ is the preferred working fluid over the entire range of analyzed operating conditions. Performance map for the bottoming ORC is presented in Figure 9C. Depending on the TC-ET, Iso-butane, R11, or ethanol are the preferred working fluids.

Thermal efficiency of a combined regenerative Brayton/ORC cycle is shown in Figure 10A. At the maximum temperature of 1000 °C, minimum topping cycle temperature of 32 °C, and P_{max} of 30 MPa, the combined Brayton/ORC cycle has a thermal efficiency of 55%. Figure 10B shows the A value given in Equation (22), i.e., the improvement in thermal efficiency of the combined regenerative Brayton/ORC cycle with respect to the regenerative Brayton cycle. Since the cycle exhaust temperature of a regenerative Brayton cycle is quite high, the rejected heat used by a bottoming ORC increases thermal efficiency of the combined cycle by up to 15%-points ($A = 0.15$). In addition, as shown in Figure 10B, efficiency improvement increases as maximum temperature of the topping cycle is increased. This is because higher maximum temperature results in a higher exhaust temperature (T_6) (see Figure 7), thus the topping cycle is providing higher temperature heat to the bottoming ORC cycle, which increases efficiency of the bottoming cycle.

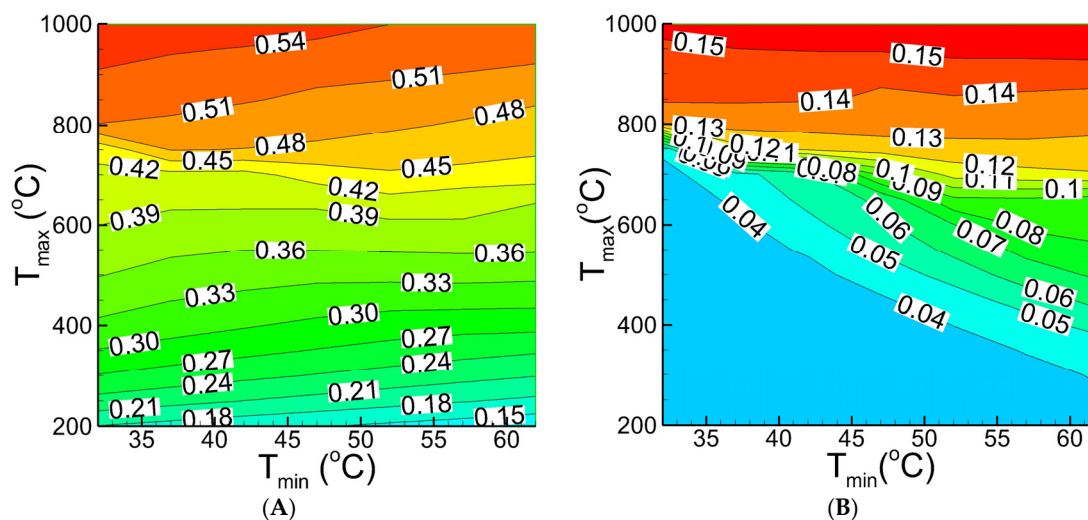


Figure 10. Thermal efficiency and A value for a combined regenerative Brayton/ORC cycle: (A) thermal efficiency; and (B) A value.

Figure 11A,B shows the net power output in MW generated by the combined regenerative Brayton/ORC cycle and the bottoming ORC, respectively. By the using waste heat from the topping cycle at T_{max} of 1000 °C, the power output of the bottoming ORC exceeds 13 MW (25% of the total power output). This is in contradiction with lines 428–429, which state that the constant power output of 100 MW was assumed for the topping cycle.

In addition, as shown in Figure 11B, for the maximum topping cycle temperatures lower than 700 °C, the minimum temperature of the topping cycle has a significant effect on the power generated by the bottoming ORC. However, for maximum temperatures higher than 700 °C, the minimum topping cycle temperature does not have a significant effect on power output of the bottoming ORC. For example, at $T_{max} = 700$ °C, increasing the minimum temperature of the topping cycle from 32 °C to 62 °C results in a 500% increase of the power output of the ORC (i.e., from 2 to 10 MW). However, at $T_{max} = 1000$ °C, increasing the minimum temperature of the topping cycle results in less than 1% increase of the net power output of the bottoming ORC.

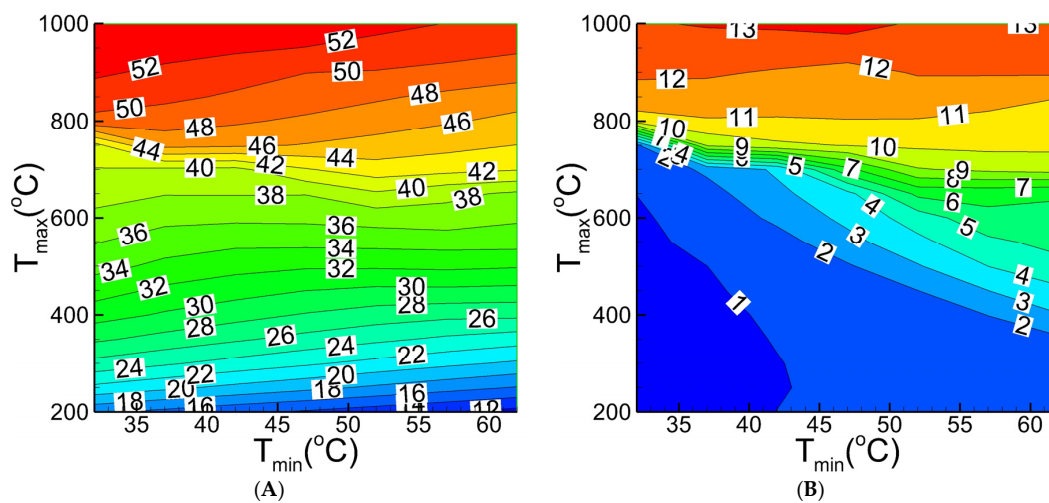


Figure 11. Net power output of the combined regenerative Brayton/ORC cycle and bottoming ORC: (A) combined Brayton/ORC cycle; and (B) bottoming ORC.

The results of the techno-economic analysis, i.e., the total capital investment, C_{TCI} , and LCOE for a combined Brayton/ORC cycle obtained over the range maximum and minimum cycle temperatures, and two maximum pressures (10 and 30 MPa), are presented in Figure 12.

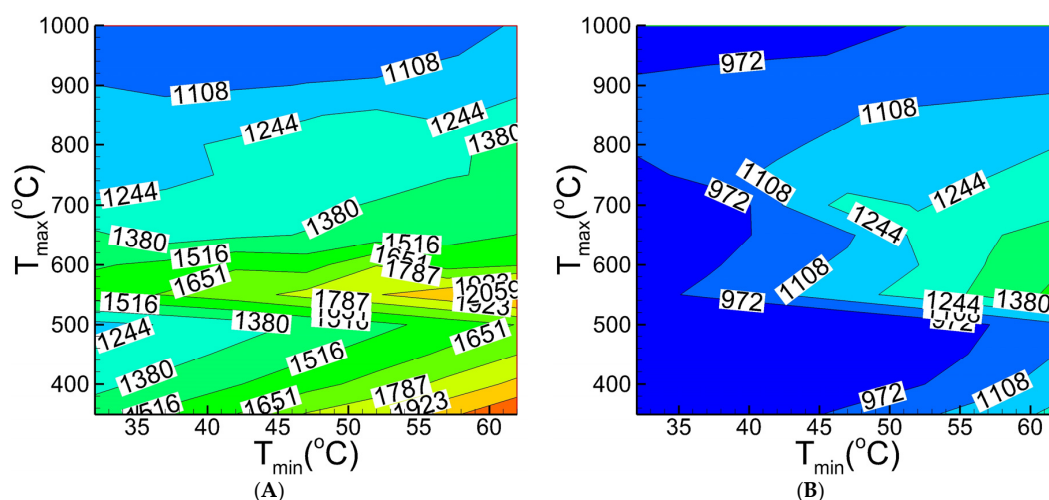


Figure 12. Cont.

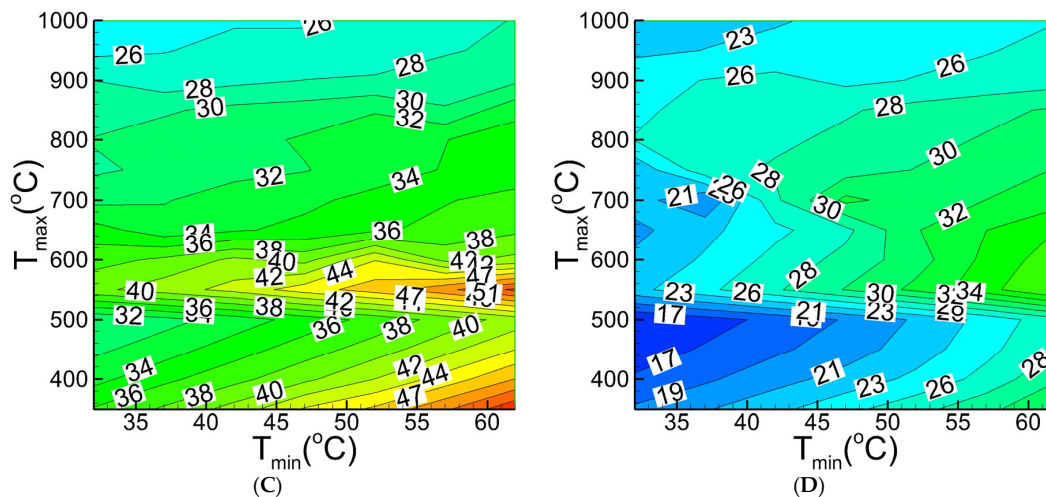


Figure 12. Total capital investment (\$/kW_{net}) and LCOE (\$/MWh) of combined Brayton/ORC cycle: (A) C_{TCI} at $P_{max} = 10$ MPa; (B) C_{TCI} at $P_{max} = 30$ MPa; (C) LCOE at $P_{max} = 10$ MPa; and (D) LCOE at $P_{max} = 30$ MPa.

As Figure 12 shows, the total capital investment and LCOE decrease as the maximum cycle pressure is increased. For example, at $T_{min} = 32$ °C, $P_{max} = 10$ MPa and $T_{max} = 1000$ °C, the total capital investment and LCOE of a combined Brayton/ORC cycle are 1000 \$/kW_{net} and 25 \$/MWh, respectively. For the same maximum and minimum temperatures and maximum pressure of 30 MPa, the values of C_{TCI} and LCOE are 940 \$/kW_{net} and 24 \$/MWh, i.e., 6 and 4 percent lower.

The effect of the maximum cycle temperature is more complex, since more expensive materials need to be used as temperature is increased, resulting in step change in cost. For example, a significant increase in total capital investment can be observed at $T_{max} = 500$ °C, since for $T_{max} > 500$ °C a more expensive stainless steel has to be used instead of carbon steel for all components of the regenerative Brayton cycle (RBC).

The total capital investment and LCOE of the CO₂ regenerative Brayton cycle (RBC) and combined Brayton/ORC cycle are compared in Figure 13 over the range of T_{max} from 300 °C to 900 °C, P_{max} of 10 and 30 MPa, and $T_{min} = 32$ °C. As the results show, the combined Brayton/ORC cycle has a significantly lower total capital investment and LCOE, compared to the regenerative Brayton cycle. For example, at $T_{max} = 550$ °C and $P_{max} = 30$ MPa, LCOE of the combined Brayton/ORC cycle is 17 \$/MWh (43%) lower compared to the RBC. As mentioned before, because of the material change, a significant increase in total capital investment and LCOE occurs at $T_{max} = 500$ °C.

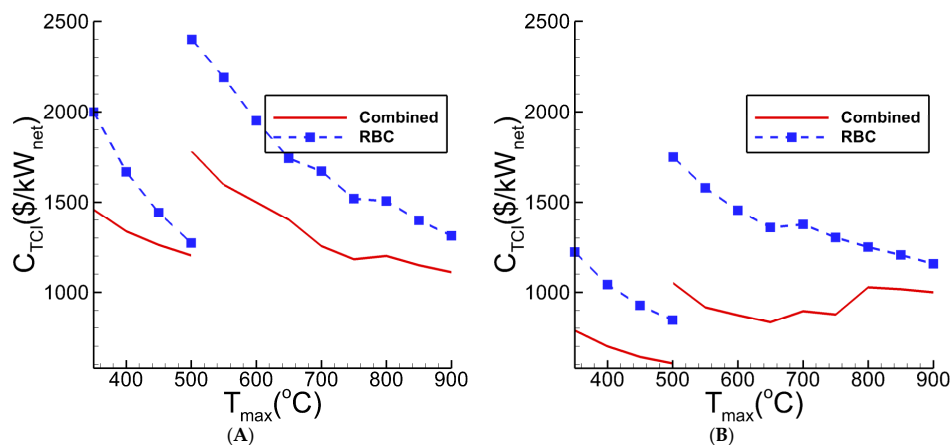


Figure 13. Cont.

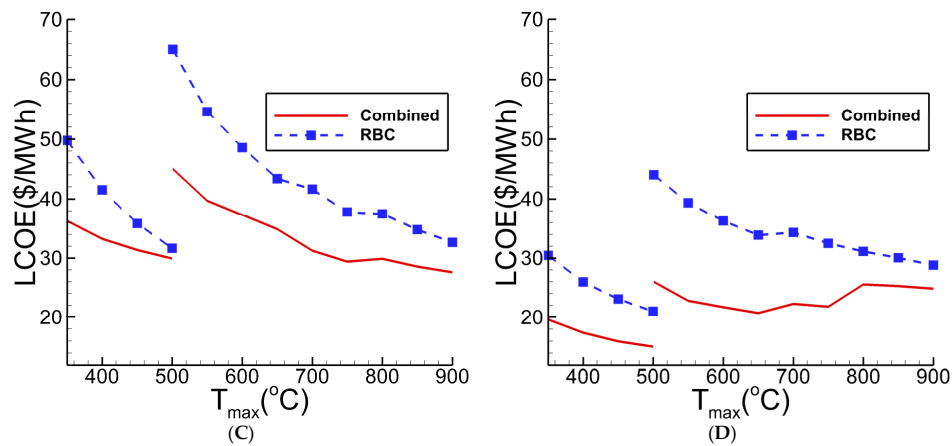


Figure 13. Total capital investment (\$/kW_{net}) and LCOE (\$/MWh) of the RBC and combined Brayton/ORC cycle: (A) C_{TCI} at $P_{max} = 10$ MPa; (B) C_{TCI} at $P_{max} = 30$ MPa; (C) LCOE at $P_{max} = 10$ MPa; and (D) LCOE at $P_{max} = 30$ MPa.

4.3. Validation of Results for the Combined Brayton/ORC Cycle

The results obtained in this study by using the EPV-11 modeling software were validated against the results published in the literature. The combined regenerative Brayton/ORC cycle utilizing CO₂ in the topping cycle and Iso-pentane in the bottoming ORC was modeled by Dunham et al. [34] using the Engineering Equation Solver (EES). Table 10 presents the cycle parameters used in the calculations. The heat input to the topping cycle is assumed to be 100 MW.

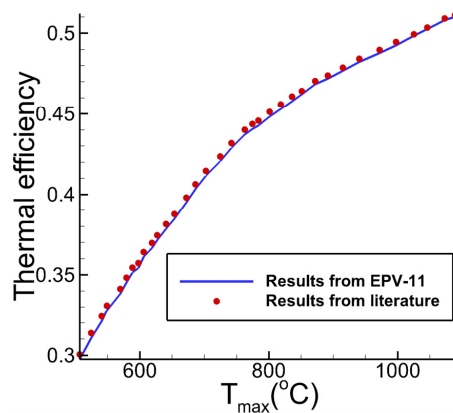


Figure 14. Thermal efficiency for different turbine inlet temperature for combined Brayton/ORC cycle.

Table 10. Cycle parameters for Combined Brayton/ORC cycle.

Parameter	Value
Compressor isentropic efficiency	0.80
Pump isentropic efficiency	0.80
Topping cycle turbine isentropic efficiency	0.9
Recuperator effectiveness	0.85
Bottoming cycle turbine isentropic efficiency	0.87
Heater pressure drop (%)	5
Minimum temperature (°C)	32
Topping cycle maximum pressure (MPa)	20

4.4. Combined steam Rankine/ORC Cycle

Steam Rankine cycle is the most widely used thermodynamic cycle for power generation. As a heat engine, it rejects large amounts of low-temperature grade heat. Its efficiency ranges from about 32% (efficiencies are given on the higher heating value (HHV) basis) for the subcritical live steam conditions, to 45% for the advanced ultra-supercritical live steam conditions [34]. Most (about 95%) of the existing power generation fleet is subcritical, about 5% is supercritical, and only a small number of the units operate at ultra-supercritical live steam conditions and efficiency of about 40% [34]. Commercial operation of the advanced ultra-supercritical units is expected within the next 10 years [48].

The efficiency of the steam Rankine cycle could be improved by addition of a bottoming cycle. Due to the low temperature of the rejected heat, the ORC is a good choice.

An analysis of a combined steam Rankine/ORC cycle was performed to determine the increase in power output that could be achieved by adding a bottoming ORC to the utility-scale (600 MW) steam Rankine cycle. The analysis included the effect of ambient conditions (heat sink temperature) on the power output of the bottoming ORC.

The analyzed utility-scale steam Rankine cycle employs a steam turbine with two double low-pressure (LP) exhausts. The steam from the LP exhausts is condensed in two steam condensers (A and B) placed in a serial arrangement, Figure 15. The cold cooling water from the cooling tower (CT) flows through condenser A first, then through condenser B. Since the temperature of the cooling water at the entrance to condenser B is higher compared to condenser A, the pressure (and saturation temperature) in condenser B is higher compared to condenser A (Table 11). The hot cooling water from condenser B is circulated back to the CT.

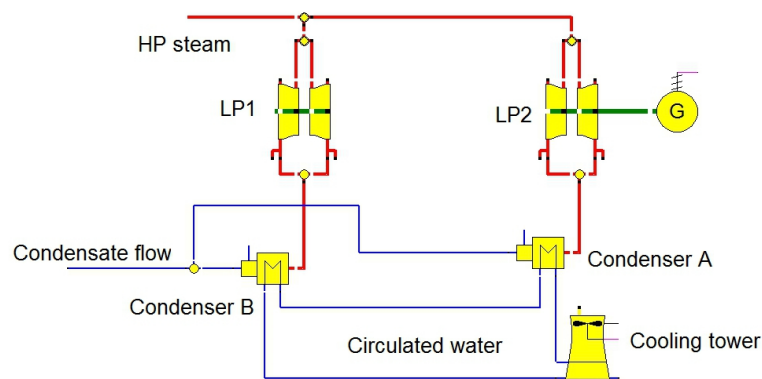


Figure 15. Schematic of the Steam Rankine cycle with two double exhaust LP turbines.

For the purpose of the analysis, it was assumed that the heat rejected in the steam condensers (latent heat of condensation) can be utilized as the heat input to the ORC. Two ORCs were employed, one for the each condenser. It was also assumed that addition of the bottoming ORC does not affect performance of the existing steam Rankine cycle because the temperature (and corresponding saturation pressure) at which heat is rejected in the condensers A and B remained the same.

Although adding a bottoming ORC to the existing steam Rankine cycle would eliminate the difference in saturation temperature and pressure between condensers A and B, the analysis was performed for conditions corresponding to the condenser A and B operating conditions to illustrate the effect of the heat source temperature. Properties of the ORC heat source used in the analysis are summarized in Table 11. In addition, the ORC analysis was performed over a range of minimum temperatures and for twelve working fluids listed in Table 1 to determine the net power output of each of the two ORCs associated with condensers (Cases) A and B. The cycle parameters used in the analysis are summarized in Table 12.

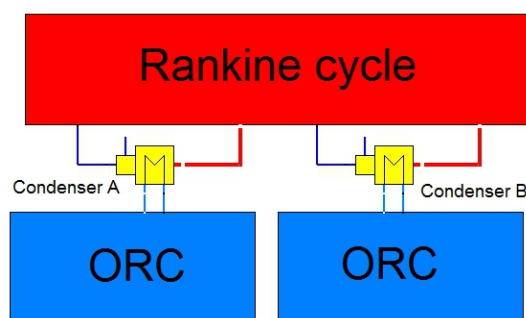
Table 11. Properties of the heat source.

Parameter	Condenser (Case) B	Condenser (Case) A
Mass flow rate of exhaust steam (kg/s)	165.63	165.63
Exhaust steam temperature (°C)	49.73	38.38
Exhaust steam pressure (MPa)	0.012	0.0067
Latent heat of evaporation (kJ/kg)	2382.5	2409.8
quality	1	1
Heat input (MW _{th})	394.89	399.13

Table 12. Cycle parameters for the bottoming ORC.

Parameter	Value	Reference
Turbine isentropic efficiency	0.87	[34]
Pump Isentropic efficiency	0.80	[34]
Minimum temperature (°C)	2–30	Assumed
Maximum pressure (MPa)	P_{sat}	Assumed

Since the condenser in the topping steam Rankine cycle would be used as the evaporator in the bottoming ORC, the steam exhausted by the LP turbine exhausts would be condensed in the ORC evaporator providing heat input to the bottoming ORC. Figure 16 shows the schematic of the combined steam Rankine/ORC cycle.

**Figure 16.** Schematic of the combined steam Rankine/ORC cycle.

Depending on the geographical location of the steam Rankine power plant, the minimum ORC temperature would follow seasonal variations. A 2 °C to 30 °C range, corresponding to the summer and winter conditions, respectively, was assumed in the analysis. The effect of the minimum temperature and working fluid on the net power output of the bottoming ORC is presented in Figure 17.

As the results presented in Figure 17 show, ethanol produces the highest power output for both cases. For Case B (heat source temperature of 49.73 °C) and minimum temperature on 2 °C, one bottoming ORC would provide additional 45 MW power output (90 MW total, or 15% of the current plant output). At the same minimum temperature, the additional power output for Case A would be 36 MW (72 MW total).

As the minimum ORC temperature increases, the power output of the ORC decreases linearly; at the minimum ORC temperature of 30 °C, the ORC power output would be 17.5 MW and 6.5 MW for Cases A and B, respectively. The lower power output is due to the smaller difference between the cycle maximum and minimum temperatures (19.73 °C and 8.38 °C) and, thus, diminishing efficiency of the ORC.

The difference in power output between R11 and R141b is negligible. Since, using R11 and ethanol has flammability and ODP issues, R141b was selected as the best working fluid for the bottoming ORC.

With R141b, the maximum additional power output generated by the ORC is 35 and 44 MW for Cases A and B, respectively.

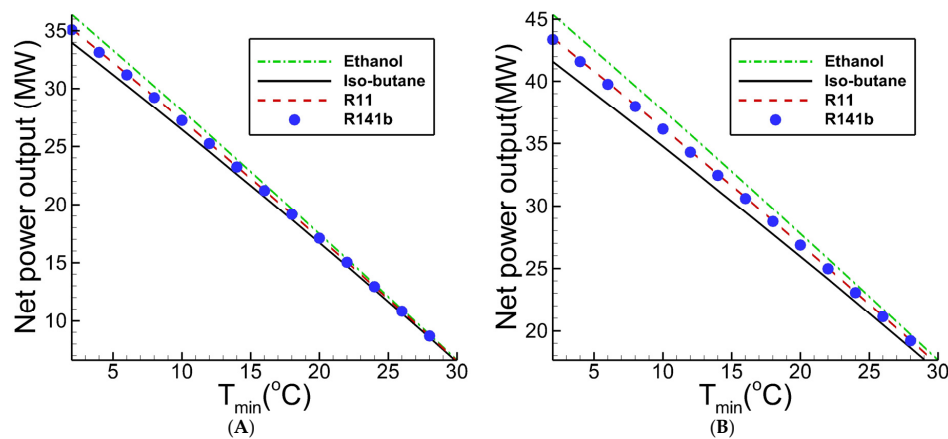


Figure 17. Net ORC power output of ORC for Cases A and B: (A) Case A; and (B) Case B.

As shown in Figure 17, during the winter when the minimum temperature is low (around 2 °C), additional power output of 70 to 88 MW can be produced by the bottoming ORC for Cases A and B, respectively. The large difference between the winter (2 °C) and summer (30 °C) temperatures has a significant effect on the ORC power output.

Although adding the bottoming ORC to the steam Rankine cycle can generate more power (i.e., the “fuel free” megawatts), it requires additional the capital investment. The capital investment for the ORC and temperature ranges used in this study is around 3000 \$/kW_{net}. A more detailed analysis is needed to determine LCOE of the Rankine/ORC cycle.

5. Conclusions

The analysis and optimization of an organic Rankine cycle (ORC) used as a bottoming cycle in the Brayton/ORC and steam Rankine/ORC combined cycle configurations was performed in this study. Parametric calculations were performed to evaluate the thermodynamic performance (thermal efficiency and net power output) of the combined Brayton/ORC cycle over a range of operating conditions. A thermodynamic analysis of the subcritical, superheated subcritical, and transcritical ORC was performed using Epsilon Professional V11 (EPV-11) power systems modeling software. A techno-economic analysis was performed for the combined Brayton/ORC cycle to determine the total capital investment and levelized cost of electricity (LCOE).

The effect of the working fluid properties on cycle performance was investigated by performing analysis for twelve working fluids. The results show that working fluids with higher specific heat capacity or latent heat of evaporation produce higher net power output in a subcritical region, while working fluids with higher specific heat capacity or latent heat of evaporation produce lower or higher thermal efficiency, respectively. In a supercritical region, working fluids with higher specific heat capacity or critical temperature produce higher thermal efficiency and net power output.

In the case of a regenerative Brayton/ORC, the results show that CO₂ and air are the best working fluids for the topping cycle. Depending on the exhaust temperature of the topping cycle, Iso-butane, R11 and ethanol are the preferred working fluids for the bottoming ORC cycle, resulting in highest efficiency of the combined cycle.

For the cycle operating conditions used in this study, the results show that, by the using the waste heat from the topping cycle, the maximum power output of the bottoming ORC exceeds 25% of the total power output, increasing thermal efficiency of the combined cycle by 15%. A performance map is constructed and presented as guidance for selection of the best working fluid(s) for the topping and bottoming cycles for the specified set of cycle operating conditions.

The results of a techno-economic analysis show that a combined Brayton/ORC cycle has significantly lower total capital investment and LCOE, compared to the regenerative Brayton cycle.

An analysis of a combined steam Rankine/ORC cycle was performed to determine the increase in power output that could be achieved by adding a bottoming ORC to the utility-scale (600 MW) steam Rankine cycle. Considering the flammability and ODP issues, R141b was selected as the best working fluid for the bottoming ORC. The total additional power output, generated by the bottoming ORC, is a strong function of the sink temperature and varies from 88 MW in the winter to 35 MW in the summer, i.e., by more than 60% for Case B.

In conclusion, recovery and utilization of waste heat in the ORC is an efficient and cost effective method for increasing power output and thermal efficiency of power cycles. The magnitude of the improvement is, however, highly dependent on the ORC sink (minimum) temperature, and the difference between the maximum and minimum operating temperatures of the ORC.

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Nomenclature

C	Cost
C_p	Specific heat [kJ/kg·K]
d	Discount rate
h	Enthalpy [kJ/kg]
h_{fg}	Latent heat [kJ/kg]
\dot{m}	Mass flow rate [kg/s]
P	Pressure [MPa]
\dot{Q}	Heat rate [kW]
r	Inflation rate
s	Specific entropy [kJ/kg·K]
T	Temperature [K]
\dot{W}	Power [kW]

Greek symbols

η	Efficiency
ε	Effectiveness

Subscript

1–10	State points in the cycle
c	Compressor
cr	Critical point
ev	Evaporation
f	Working fluid
in	Inlet
max	Maximum
md	modified
min	Minimum
net	Net
p	Pump
r	Dimensionless
reg	Regeneration
t	Turbine
th	Thermal

Acronyms

EPV-11	Epsilon Professional V11
FOM	Figure of merit
GWP	Global warming potential
Ja	Jacob number
ODP	Ozone depletion potential
ORC	Organic Rankine cycle
TCI	Total capital investment
TIT	Turbine inlet temperature
LCOE	Levelized cost of electricity

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